# **PCT**

# WORLD INTELLECTUAL PROPERTY ORGANIZATION International Bureau



# INTERNATIONAL APPLICATION PUBLISHED UNDER THE PATENT COOPERATION TREATY (PCT)

(51) International Patent Classification 5:		(11) International Publication Number:	WO 95/14734
C08K 5/15, C08J 5/18	A1	(43) International Publication Date:	1 June 1995 (01.06.95)
(21) International Application Number: PCT/US9 (22) International Filing Date: 16 November 1994 (1)		(AT, BE, CH, DE, DK, ES, FR, GE	
(30) Priority Data: 157,546 26 November 1993 (26.11.9)	3) (	Published  With international search rept.	
(71) Applicant: EASTMAN CHEMICAL COMPANY   100 North Eastman Road, Kinsport, TN 37660 (U.		3:	
(72) Inventors: SHIH, Wayne, Keng; 1032 Norfold Kingsport, TN 37660 (US). LIGHT, Ronald, Rich Whitehaven Drive, Kingsport, TN 37660 (US).			
(74) Agent: THALLEMER, John, D.; P.O. Box 511, Kings 37662-5075 (US).	sport, T	N	
_			
(54) Title: PLASTICIZED POLYESTER FOR SHRINK I	FILM .	APPLICATIONS	

### (57) Abstract

This invention relates to polyester/plasticizer blends which are useful as heat-shrinkable films or sheet in low temperature shrink packaging applications. The plasticizer is injected into the melt of the polyester. The plasticizer lowers the glass transition temperature, on-set temperature and shrink rate of the polyester. Film or sheet produced by the polyester/plasticizer blends is clear.

### FOR THE PURPOSES OF INFORMATION ONLY

Codes used to identify States party to the PCT on the front pages of pamphlets publishing international applications under the PCT.

Austria	GB	United Kingdom	MIR	Mauritania
	GE	Georgia	MW	Malawi
	GN	Guinea	NE	Niger
	GR	Greece	NL	Netherlands
	HU	Hungary	NO	Norway
		Ireland	NZ	New Zealand
•	IT	Italy	PL.	Poland
	JP		PT	Portugal
	KE	•	RO	Romania
	KG		RU	Russian Federation
	KP		SD	Sudan
•		of Korea	SE	Sweden
_	KR	Republic of Korea	SI	Slovenia
		Kazakhstan	SK	Slovakia
		Liechtenstein	SN	Senegal
		Sri Lanka	TD	Chad
-			TG	Togo
		_	TJ	Tajikistan
=			TT	Trinidad and Tobago
			UA	Ukraine
		•	US	United States of America
-		_	UZ	Uzbekistan
- <del> </del>			_	Viet Nam
		*.************************************	• • • • • • • • • • • • • • • • • • • •	
	Austria Australia Barbados Belgium Burkina Faso Bulgaria Benin Brazil Belarus Canada Central African Republic Congo Switzerland Cate d'Ivoire Cameroon China Czechoelovakia Czech Republic Germany Demark Spain Finland France Gabon	Australia GE Barbados GN Belgium GR Burkina Faso HU Bulgaria IE Benin IT Brazil JP Belarus KE Canada KG Central African Republic KP Congo Switzerland KR Cote d'Ivoire KZ Cameroon LI China LK Czechoslovakia LU Czech Republic LV Germany MC Demark MD Spain MG Finland ML France MN	Australia GE Georgia Barbados GN Guinea Belgium GR Greece Burkina Paso HU Hungary Bulgaria IE Ireland Benin IT Italy Brazil JP Japan Belarus KE Kenya Canada KG Kyrgystan Central African Republic KP Democratic People's Republic Congo of Korea Switzerland KR Republic of Korea Cote d'Ivoire KZ Kazakhstan Cameroon LI Liechtenstein China Case Cechoslovakia LU Luxembourg Czech Republic LV Larvia Germany MC Monaco Demark MD Republic of Moldova Spain MG Madagascar Finland MI Mail Prance MN Mongolia	Australia GE Georgia MW Barbados GN Guinea NE Belgium GR Greece NL Burkina Paso HU Hungary NO Bulgaria IE Ireland NZ Benin IT Italy PL Brazil JP Japan PT Belarus KE Kenya RO Canada KG Kyrgystan RU Central African Republic KP Democratic People's Republic SD Congo of Korea SE Switzerland KR Republic of Korea SI Cote d'Ivoire KZ Kazakhsan SK Cameroon LI Lieckhenstein SN China LK Sri Lanka TD Czechoslovakia LU Luxembourg TG Czech Republic LV Latvia TJ Germany MC Monaco TT Demarrk MD Republic of Moldova UA Spain MG Madagascar US Finland ML Mait UZ France MN Mongolia

5

10

30

35

- 1 -

#### PLASTICIZED POLYESTER FOR SHRINK FILM APPLICATIONS

#### FIELD OF THE INVENTION

This invention relates to polyester/plasticizer blends which are useful as heat-shrinkable films or sheet in low temperature shrink packaging applications. The plasticizer is injected into the melt of the polyester. The plasticizer lowers the glass transition temperature, on-set temperature and shrink rate of the polyester. Film or sheet produced by the polyester/plasticizer blends is clear.

#### BACKGROUND OF THE INVENTION

Heat-shrinkable plastic films are used for 15 labelling, protection, parceling, and wrapping of glass, metal, ceramic and plastic bottles, boxes, cans, pipes, and wood. For example, heat-shrinkable films are widely used as tamper evident labels on food and pharmaceutical products and as primary labels on plastic containers 20 such as soft drink bottles. Shrink films are classified into two categories: (1) biaxially oriented film for wrapping wherein the film shrinks in both the x- and vaxis directions, and (2) uniaxially oriented film wherein the film primarily shrinks in the stretched or 25 oriented direction and has a little shrinkage in the unstretched or nonoriented direction.

The most widely used shrink film is polyvinylchloride (PVC), however, shrink films have been prepared from polystyrene (OPS), oriented polyethylene, oriented polypropylene, and polyesters. While PVC has good at-shrinkable properties, PVC is not suitable for low temperature shrink packaging. In addition, the incineration of PVC g nerates hydrogen chloride which causes corrosion of the incinerator and environmental pollution.

5

10

15

20

25

30

35

- 2 -

Example of a heat-shrinkable polyester film are disclosed in U.S. Pat. Nos. 4,996,291 and 4,963,418.

U.S. Pat. No. 4,996,291 discloses a heat-shrinkable polyester film prepared from polyethylene terephthalate. While a list of additives is included, plasticizers are not listed. U.S. Pat. No. 4,963,418 discloses a heat-shrinkable polyester film prepared from a polyester, a polyester copolymer, or a mixture of a polyester and a polyester copolymer. No suggestion is made of forming a blend with a plasticizer or any other additive.

Previously disclosed polyester films have at least two major disadvantages, a higher on-set shrink temperature than 50-60°C and a higher shrink rate than 4% per degree celsius. A high on-set shrink temperature means that the film or sheet requires a higher temperature at which the film starts to contract in a heated shrink tunnel or oven. High on-set temperature can cause container or content damage. The other disadvantage is a higher shrink rate which refers to the percent shrinkage per degree of temperature increase. A high shrink rate causes wrinkle or bubble formation in shrink film or sheet as it travels through the shrink tunnel.

The present inventors have unexpectedly determined that the on-set shrink temperature and the shrink rate of a heat-shrinkable film or sheet prepared from a polyester can be decreased by melt blending a critical amount of a plasticizer selected from a C<sub>4</sub> to C<sub>20</sub> alkyl ester of an epoxidized fatty acid having 12 to 20 carbon atoms provided the plasticizer has sufficient stability to permit its incorporation into the polyester at a temperature of 200°C to 300°C. Moreover, th polyest r/plasticizer blends of the present invention produce cl ar film without the environmental disadvantages associated with other films.

**- 3 -**

### SUMMARY OF THE INVENTION

Accordingly, it is one object of the present invention to provide a heat—shrinkable film which is environmentally safe and does not contain the disadvantages associated with previous heat shrinkable films.

5

10

20

25

30

35

Accordingly, it is another object of the invention is to provide heat shrinkable films with lower on-set temperature and lower shrink rate than heat-shrinkable films prepared from polyvinylchloride.

Accordingly, it is a further object of the invention to provide a process for preparing heat sh nkable films wherein the on-set temperature can be modified to meet individual specifications.

Still another object of the invention is to provide heat—shrinkable films which exhibit resistance to heat, printability, impact resistance, and stress crack resistance, and which display excellent melt flowability at the time of extr ion thereof.

These and other objects are accomplished herein by a heat-shrinkable film comprising a blend of:

- (A) 90 to 99 weight percent of a polyester having a glass transition temperature of 40°C to 150°C and an inherent viscosity of 0.5 to 1.2 dL/g, comprising
- (1) a dicarboxylic acid component comprising repeat units from at least 80 mole percent of an aromatic dicarboxylic acid having 8 to 14 carbon atoms, and
- (2) a diol component comprising repeat units from at least 1 mole percent of 1,4—cyclohexanedimethanol, based on 100 mole percent dicarboxylic acid and 100 mole percent diol; and
- (B) 1 to 10 weight perc nt of a plasticizer selected from a  $C_4$  to  $C_{20}$  alkyl ester of an epoxidized fatty acid having 12 to 20 carbon atoms provid d the plasticizer has sufficient stability to permit its

5

10

15

20

25

30

35

incorporation into the polyester at a temperature of 200°C to 300°C, wherein the combined weights of (A) and (B) total 100 percent.

#### DESCRIPTION OF THE INVENTION

The polyester, component (A), of the present invention includes copolyesters. The polyester may be semi-crystalline or amorphous, preferably amorphous. The polyester contains repeat units from a dicarboxylic acid and a diol, based on 100 mole percent dicarboxylic acid and 100 mole percent diol. The dicarboxylic acid component contains at least 80 mole percent of an aromatic dicarboxylic acid having 8 to 14 carbon atoms. The polyester may optionally be modified with up to 20 mole percent, based on 100 mole percent dicarboxylic acid, of one or more different dicarboxylic acids other than an aromatic dicarboxylic acid, such as saturated aliphatic dicarboxylic acids having 4 to 12 carbon atoms and cycloaliphatic dicarboxylic acids having 8 to 12 carbon atoms. Specific examples of dicarboxylic acids are: terephthalic acid, phthalic acid, isophthalic acid, naphthalene-2,6-dicarboxylic acid, cyclohexanedicarboxylic acid, cyclohexanediacetic acid, diphenyl-4,4'-dicarboxylic acid, succinic acid, glutaric acid, adipic acid, azelaic acid, sebacic acid, and the like. The polyester may be prepared from one or more of the above dicarboxylic acids.

It should be understood that use of the corresponding acid anhydrides, esters, and acid chlorides of these acids is included in the term "dicarboxylic acid".

The diol comp nent c ntains repeat units from at least 10 mole p rcent 1,4—cyclohexanedimethanol. In additi n, th diol c mp nent can ptionally be modified with up to 90 mole percent, based on 100 mole percent

25

30

35

diol, of one or more different diols other than 1,4-cyclohexanedimethanol. Such additional diols include cycloaliphatic diols having 6 to 15 carbon atoms and aliphatic diols having 3 to 8 carbon atoms.

- Examples of such diols to be included with 1,4-cyclohexanedimethanol are: ethylene glycol, diethylene glycol, triethylene glycol, propane-1,3-diol, butane-1,4-diol, 2,2-dimethylpropane-1,3-diol (neopentyl glycol), pentane-1,5-diol, hexane-1,6-diol, 3-
- methylpentanediol-(2,4), 2-methylpentanediol-(1,4),
  2,2,4-trimethylpentane-diol-(1,3),
  2-ethylhexanediol-(1,3), 2,2-diethylpropane-diol-(1,3),
  hexanediol-(1,3), 1,4-di-(hydroxyethoxy)-benzene,
  2,2-bis-(4-hydroxycyclohexyl)-propane,
- 2,4-dihydroxy-1,1,3,3-tetramethyl-cyclobutane,
  2,2-bis-(3-hydroxyethoxyphenyl)-propane,
  2,2-bis-(4-hydroxypropox nenyl)-propane, and the like.
  The polyester may be prepared from one or more of the above diols.
- The polyester may also contain small amounts of trifunctional or tetrafunctional comonomers such as trimellitic anhydride, trimethylolpropane, pyromellitic dianhydride, pentaerythritol, and other polyester forming polyacids or polyols generally known in the art.

For the purposes of the present invention, the preferred polyester, component (A), has a dicarboxylic acid component consisting of repeat units from terephthalic acid and a diol component consisting of repeat units from 65 to 90 mole percent ethylene glycol and 35 to 10 mole percent 1,4-cyclohexanedimethanol. More preferably, the diol portion consists of 67 to 75 mole p rcent ethylen glycol and 33 to 25 mole percent 1,4-cyclohexanedimethan 1.

P lyesters useful as component (A) have an inherent viscosity of 0.5 to 1.2 dL/g. Preferably, the poly st r

5

10

15

20

25

30:

35

- 6 -

has an inherent viscosity of 0.6 to 0.9 dL/g as measured at 25°C. using 0.50 grams of polymer per 100 ml of a solvent consisting of 60% by weight phenol and 40% by weight tetrachloroethane. Polyesters useful as component (A) also have a glass transition temperature of 40°C to 150°C, preferably 50°C to 100°C.

The polyester may be prepared by conventional polycondensation procedures well-known in the art. Such processes include direct condensation of the dicarboxylic acid(s) with the diol(s) or by ester interchange using a dialkyl dicarboxylate. For example, a dialkyl terephthalate such as dimethyl terephthalate is ester interchanged with the diol(s) at elevated temperatures in the presence of a catalyst. The polyesters may also be subjected to solid state polymerization methods.

Component (B) of the present invention is a plasticizer. Plasticizers useful as component (B) are selected from a  $C_4$  to  $C_{20}$  alkyl ester of an epoxidized fatty acid having 12 to 20 carbon atoms. plasticizer should have sufficient stability to permit its incorporation into the polyester at a temperature of 200°C to 300°C, preferably, 250°C to 280°C. The term "sufficient stability" means that the plasticizer should be stable to decomposition and volatility within a temperature range of 200°C to 300°C. Examples of suitable plasticizers include: octyl epoxy soyate, epoxidized soybean oil, epoxy tallates, epoxidized linseed oil, triphenyl phosphate, neopentyl glycol dibenzoate, glycerine, vegetable oil, caster oil, and mineral oil. Preferably, the plasticizer is octyl epoxy soyate which is c mmercially available under the tradename VIKOFLEX 7080 from Elf At chem.

Th pr cess for preparing the polyester/plasticizer blends of the present invention involve preparing the

5

10

15

20

25

30

35

- 7 -

polyester by a process as mentioned previously. The polyester is dried in an atmosphere of dried air or dried nitrogen, or under reduced pressure. Under melt processing conditions the polyester undergoes molecular weight degradation in the presence of contaminants such as water, thus, it is preferable that the polyester be incorporated in anhydrous form into the blends of the present invention.

The plasticizer is mixed with the polyester by any suitable melt blending process such as batch mixing, single screw, or twin screw extrusion. Preferably, the plasticizer is injected into the melt of the polyester using a liquid or solid pumping system. The polyester/plasticizer blends may also be prepared by adding the plasticizer to the polyester late in the polymerization after polymerization is essentially complete. After completion of the melt compounding, the extrudate is withdrawn in strand form, and recovered according to the usual way such as cutting.

The extrudate, prepared above, may be used as a concentrate which is mixed with the polyester, component (A). Methods for mixing the concentrate pellets with the polyester pellets include feeding the concentrate pellets with an additive feeder and mechanically mixing the polyester and concentrate pellets. The polyester/concentrate blends are melt blended, dried and extruded into a film or sheet.

The percentage by weight of the polyester in the polyester/plasticizer blend is 90 to 99%. More preferably, the polyester constitutes 94 to 98 weight percent of the polyester/plasticizer blend. The polyester/plasticizer blends of the present invention have an inher nt viscosity of 0.55 dl/g to 1.5 dl/g, preferably 0.70 to 0.80 dl/g as measured at 23°C using 0.50 grams of polymer per 100 ml f a solvent consisting

- 8 -

of 60% by weight phenol and 40% by weight tetrachloroethane.

5

10

15

20

25

30

35

Many other ingredients can be added to the compositions of the present invention to enhance the performance properties of the blends. For example, denesting agents, anti-blocking agents, stabilizers, antioxidants, ultraviolet light absorbing agents, mold release agents, metal deactivators, colorants such as titanium dioxide and carbon black, granulated silica, kaolin, calcium carbonate, anti-static agents, fillers, and the like, can be included herein. All of these additives and the use thereof are well known in the art and do not require extensive discussions. Therefore, only a limited number will be referred to, it being understood that any of these compounds can be used so long as they do not hinder the present invention from accomplishing its objects.

The polyester/plasticizer blends of the present invention serve as excellent starting materials for the production of films of all types especially heat-shrinkable films and sheet. Heat-shrinkable plastic films are used for labelling, protection, parceling, and wrapping of glass, metal, ceramic and plastic bottles, boxes, cans, pipes, and wood. For example, heat-shrinkable films are widely used as tamper evident labels on food and pharmaceutical products, as primary labels on plastic containers such as soft drink bottles, and protective wraps for medicines and dry cell batteries.

The materials and testing procedures used for the results shown herein are as follows:

Haze was determined by ASTM D1003. Haze values of less than 5% are acceptable for clear sheet or film.

Maximum shrink rat is defined as the maximum first derivativ or sl pe of the shrink curve and indicates

- 9 -

how fast the film will contract when it is heated in an oven or tunnel.

On-set shrink temperature is the temperature at which the film shrinks 2%.

The invention will be further illustrated by a consideration of the following examples, which are intended to be exemplary of the invention. All parts and percentages in the examples are on a weight basis unless otherwise stated.

10

15

20

25

30

5

#### EXAMPLE I

Polyester pellets consisting of 100 mole percent terephthalic acid, 65-70 mole percent ethylene glycol and 30-35 mole percent 1,4-cyclohexanedimethanol with an I.V. of 0.75 was dried at 65°C. for 4 hours in desiccant air with a dew point ≤-29°C. The PETG polyester was placed in the hopper of a single screw extruder and extruded into 5-10 ml sheets at 260°C.

The polyester had an I.V. of 0.73 dl/g and a Tg, as determined by DSC at 20°C/min, of 77°C. The test results of the PETG polyester are summarized in Table I.

#### EXAMPLE II

Sheet prepared from 98 wt% PETG polyester and 2 wt% octyl epoxy soyate.

A polyester/plasticizer concentrate was prepared using 10 weight percent of liquid octyl epoxy soyate and 90 weight percent of the PETG polyester pellets prepared in Example I. The concentrate pellets were mechanically blended with PETG polyester pellets from Example I in a ratio of 20/80, respectively. The pellets were extruded into a sheet using a single screw xtruder.

Th final concentration f ctyl epoxy soyate in the sheet was 2 weight percent. The plymer had a Tg,

- 10 -

as determined by DSC at 20°C/min, of 67°C. The test results are summarized in Table I.

#### EXAMPLE III

Sheet prepared from 96 wt% PETG copolyester and 4 wt% octyl epoxy soyate.

10

15

25

30

A polyester/plasticizer concentrate was prepared using 10 weight percent of liquid octyl epoxy soyate and 90 weight percent of the PETG polyester pellets prepared in Example I. The concentrate pellets were mechanically blended with PETG polyester pellets from Example I in a ratio of 40/60, respectively. The pellets were extruded into a sheet using a single screw extruder.

The final concentration of octyl epoxy soyate in the sheet was 4 weight percent. The polymer had a Tg, as determined by DSC at 20°C/min, of 61°C. The test results are summarized in Table I.

#### EXAMPLE IV

Sheet prepared from 94 wt% PETG copolyester and 6 wt% octyl epoxy soyate.

A polyester/plasticizer concentrate was prepared using 10 weight percent of liquid octyl epoxy soyate and 90 weight percent of the PETG polyester pellets prepared in Example I. The concentrate pellets were mechanically blended with PETG polyester pellets from Example I in a ratio of 60/40, respectively. The pellets were extruded into a sheet using a single screw extruder.

The final concentration of octyl epoxy soyate in the sheet was 6 weight percent. The polymer had a Tg, as determined by DSC at 20°C/min, of 54°C. The test results are summarized in Table I.

- 11 -

#### EXAMPLE V

Sheet prepared from 92 wt% PETG copolyester and 8 wt% octyl epoxy soyate.

A polyester/plasticizer concentrate was prepared using 10 weight percent of liquid octyl epoxy soyate and 90 weight percent of the PETG polyester pellets prepared in Example I. The concentrate pellets were mechanically blended with PETG polyester pellets from Example I in a ratio of 80/20, respectively. The pellets were extruded into a sheet using a single screw extruder.

The final concentration of octyl epoxy soyate in the sheet was 8 weight percent. The polymer had a Tg, as determined by DSC at 20°C/min, of 49°C. The test results are summarized in Table I.

15

20

25

10

5

#### EXAMPLE VI

Sheet prepared from 90 wt% PETG copolyester and 10 wt% octyl epoxy soyate.

A polyester/plasticizer concentrate was prepared using 10 weight percent of liquid octyl epoxy soyate and 90 weight percent of the PETG polyester pellets prepared in Example I. The concentrate pellets were mechanically blended with PETG polyester pellets from Example I in a ratio of 90/10, respectively. The pellets were extruded into a sheet using a single screw extruder.

The final concentration of octyl epoxy soyate in the sheet was 10 weight percent. The polymer had a Tg, as determined by DSC at 20°C/min, of 42°C. The test results are summarized in Table I.

- 12 -

TABLE I

EXAMPLE	POLYESTER (wt%)	PLASTICIZER (wt%)	Tg (°C)	HAZE
ī	100	0	77°C	0.39
II	98	2	67°C	0.62
III	96	4	61°C	0.68
IV	94	6	54°C	0.65
v	92	8	49°C	
VI	90	10	42°C	

10

15

5

The results in Table I clearly show that the glass transition temperature of a heat-shrinkable polyester film can be significantly decreased by melt blending a critical amount of a plasticizer having low volatility at a temperatures of less than 300°C with the polyester. In addition, the haze values indicate that the film produced by the polyester/plasticizer blends of the present invention are clear since the percent haze is significantly below 5%.

20

25

#### EXAMPLE VII

PVC sheet was stretched into film at 90°C with a stretch ratio 3 times in the machine direction (MD) and without any stretch in the transverse direction (TD). In other words, the film was uniaxially oriented. The shrinkage of the oriented film was measured in a constant temperature water bath for 30 seconds. Typical data measured at 60, 70, 80, and 90°C respectively are illustrated in Table II. The on—set shrink temperature was about 60°C. The maximum shrink rate is the highest first derivative value, slope, of shrinkage vs temperature curve or shrink curve. The test results for PVC shrinkag and maximum shrink rat are summarized in Table II.

- 13 -

#### EXAMPLE VIII

The PETG polyester prepared in Example I was extruded into sheet then stretched into film at 90°C with a MD stretch ratio 4 times. The on-set shrink temperature for PETG was about 65°C. The test results for PETG shrinkage, maximum shrink rate and mechanical properties are summarized in Tables II and III.

#### EXAMPLE IX

The PETG polyester pellets prepared in Example I were melt blended with 2% octyl epoxy soyate and extruded into sheet then stretched into film at 85°C with a MD stretch ratio 4 times. The test results for shrinkage, maximum shrink rate and mechanical properties are summarized in Tables II and III.

#### EXAMPLE X

The PETG polyester pellets prepared in Example I were melt blended with 4% octyl epoxy soyate and extruded into sheet then stretched into film at 80°C with a MD stretch ratio 4 times. The test results for shrinkage, maximum shrink rate and mechanical properties are summarized in Tables II and III.

25 EXAMPLE XI

5

20

30

The PETG polyester pellets prepared in Example I were melt blended with 6% octyl epoxy soyate and extruded into sheet then stretched into film at 75°C with a MD stretch ratio 4 times. The test results for shrinkage, maximum shrink rate and mechanical properties are summarized in Tables II and III.

- 14 -

#### EXAMPLE XII

The PETG polyester pellets prepared in Example I were melt blended with 8% octyl epoxy soyate and extruded into sheet then stretched into film at 70°C with a MD stretch ratio 4 times. The on-set temperature of the shrink film was so low that the film began shrinking during a warm day.

5

30

35

#### EXAMPLE XIII

The PETG polyester pellets prepared in Example I were melt blended with 10% octyl epoxy soyate and extruded into sheet then stretched into film at 65°C with a MD stretch ratio 4 times. The on-set temperature of the shrink film was so low that the film began shrinking during a warm day.

TABLE II

	EXAMPLE	VII	VIII	IX	Х	XI
	Stretch Temp, °C	90	90	85	80	75
20	Stretch Ratio	3	4	4	4	4
	Shrinkage at 60°C, %	2	0	2	11	27
	Shrinkage at 70°C, %	26	21	29	52	49
	Shrinkage at 80°C, %	51	63	66	70	58
	Shrinkage at 90°C, %	58	73	75	75	70
25	Max. Shrink Rate, %/°C	3.90	5.22	4.28	3.90	3.75
	On Set Shrink Temp. °C	60	65	60	55	45

The results in Table II clearly show that both on-set shrink temperature and maximum shrink rate are reduced by modification with a plasticizer. In addition, the data indicates that PETG is inferior to PVC since PETG has a higher maximum shrink rate and on-set shrink temperature.

The polyester/2% plasticizer blend has 2% shrinkage at 60°C as compared to 0% for straight PETG. The

PCT/US94/13127

5

10

15

20

maximum shrink rate also decreases from 5.22 %/°C of straight PETG to 4.28%/°C of plasticized PETG with 2% Therefore, the on-set shrink temperature of plasticized PETG with 2% OES is identical to that of PVC even though its maximum shrink rate is still higher than that of PVC.

The polyester/4% plasticizer blend has an on-set shrink temperature of about 55°C. It has 11% shrinkage at 60°C and the maximum shrink rate of this plasticized PETG is 3.9%/°C which is identical to that of PVC. short, the plasticized PETG with 4% OES has the similar shrink rate as compared to PVC. It has lower on-set shrink temperature so that it can be used in even lower temperature shrink packaging. This plasticized version of PETG has even better shrinkage characteristics compared to straight PETG 6763.

The polyester/6% plasticizer blend has an on-set shrink temperature of about 45°C which is suitable for very heat sensitive shrink packaging. The maximum shrink rate is also reduced to 3.75%/°C.

					= :	
				BLE III Properties		
	EXAMPLE		VIII	IX	x	IX
	Yield Stress	MD	151.3	111.6	82.3	60.3
5	(MPa)	TD	53	36.8	36.4	36.9
	Yield strain	MD	5.6	5.4	5.1	5.0
	(%)	TD	3.4	3.6	4.3	5.4
10	Young Mod.	MD	5530	3841	2661	1793
	(MPa)	TD	1805	1280	1207	1241
	Stiffness	MD	108	136	84	69
15	$(N. mm/cm^3)$	TD	250	167	136	102
13	Break stress	MD	382.3	271.6	179.1	102.8
	(MPa)	TD	80.4	49.6	39.3	27.9
	Break strain	MD	46.1	88.1	78.3	107.2
20	(%)·			466		351.2
	MD - machine					
	TD - transvers	se di:	rectio:	r unoriente	ed direction	מכ

PCT/US94/13127

**- 16 -**

The data in Table III indicates that the polyester/plasticizer blends of the present invention produce heat—shrinkable films and sheet which exhibit acceptable mechanical properties.

- 17 -

#### WHAT IS CLAIMED IS:

- 1. A heat-shrinkable film comprising a blend of:
- (A) 90 to 99 weight percent of a polyester having a glass transition temperature of 40°C to 150°C and an inherent viscosity of 0.5 to 1.2 dL/g, comprising
- (1) a dicarboxylic acid component comprising repeat units from at least 80 mole percent of an aromatic dicarboxylic acid having 8 to 14 carbon atoms, and
- (2) a diol component comprising repeat units from at least 10 mole percent of 1,4-cyclohexanedimethanol, based on 100 mole percent dicarboxylic acid and 100 mole percent diol; and
- (B) 1 to 10 weight percent of a plasticizer selected from a C<sub>4</sub> to C<sub>20</sub> alkyl ester of an epoxidized fatty acid having 12 to 20 carbon atoms provided the plasticizer has sufficient stability to permit its incorporation into the polyester at a temperature of 200°C to 300°C, wherein the combined weights of (A) and (B) total 100 percent.

20

25

30

35

15

5

. 10

- 2. A heat-shrinkable film comprising a blend of:
- (A) 90 to 99 weight percent of a polyester having a glass transition temperature of 40°C to 150°C and an inherent viscosity of 0.5 to 1.2 dL/g, comprising
- (1) a dicarboxylic acid component comprising repeat units from at least 80 mole percent of terephthalic acid, and
  - (2) a diol component comprising repeat units from 65 to 90 mole percent ethylene glycol and 35 to 10 mole percent 1,4-cyclohexanedimethanol, based on 100 mole percent dicarboxylic acid and 100 mole percent diol; and
  - (B) 1 to 10 weight percent of a plasticizer sel cted from the group consisting of octyl epoxy soyate, epoxy tallates, epoxidized soybean oil,

epoxidized linseed oil, triphenyl phosphate, neopentyl glycol dibenzoate, glycerine, vegetable oil, and mineral oil, wherein the combined weights of (A) and (B) total 100 percent.

5

- 3. The heat-shrinkable film of Claim 2 wherein the dicarboxylic acid component of the polyester consists essentially of repeat units from terephthalic acid.
- 4. The heat-shrinkable film of Claim 2 wherein the diol component of the polyester consists essentially of repeat units from 67 to 75 mole percent of ethylene glycol and 33 to 25 mole percent of 1,4-cyclohexanedimethanol.

15

5. The heat-shrinkable film of Claim 1 wherein the plasticizer, component (B), is present in an amount f 2 to 6 weight percent based on the weight of components (A) and (B).

20

6. The heat-shrinkable film of Claim 2 wherein the plasticizer, component (B), is present in an amount of 2 to 6 weight percent based on the weight of components (A) and (B).

25

- 7. The heat—shrinkable film of Claim 2 wherein the plasticizer, component (B), is octyl epoxy soyate.
- 8. The polyester of Claim 1 wherein the polyester, component (A), has an inherent viscosity of 0.6 to 0.9 dL/g.
  - 9. The p lyest r f Claim 2 wherein the polyester, component (A), has an inherent viscosity of 0.6 to 0.9 dL/g.

- 19 -

- 10. The polyester of Claim 1 wherein the polyester, component (A), has a glass transition temperature of 50°C to 100°C.
- 5 11. The polyester of Claim 2 wherein the polyester, component (A), has a glass transition temperature of 50°C to 100°C.
- 12. A process for preparing a heat-shrinkable film10 comprising:
  - (I) mixing at a temperature of 200°C to 315°C
  - (A) 90 to 99 weight percent of a polester having a glass transition temperature of 40°C to .50°C and an inherent viscosity of 0.5 to 1.2 dL/g, comprising
- 15 (1) a dicarboxylic acid component comprising repeat units from at least 80 mole percent of an aromatic dicarboxylic acid having 8 to 14 carbon atoms, and
  - (2) a diol component comprising repeat units from at least 10 mole percent of 1,4-cyclohexanedimethanol, based on 100 mole percent dicarboxylic acid and 100 mole percent diol; and
  - (B) 1 to 10 weight percent of a plasticizer selected from a C<sub>4</sub> to C<sub>20</sub> alkyl ester of an epoxidized fatty acid having 12 to 20 carbon atoms provided the plasticizer has sufficient stability to permit its incorporation into the polyester at a temperature of 200°C to 300°C, wherein the combined weights of (A) and (B) total 100 percent; and
    - (II) forming the blend into a film.

20

PCT/US94/13127

5

10

25

30

- 13. A process for preparing a heat-shrinkable film comprising:
- (I) mixing at a temperature of 200°C to 315°C
- (A) 90 to 99 weight percent of a polyester having a glass transition temperature of 40°C to 150°C and an inherent viscosity of 0.5 to 1.2 dL/g, comprising
- (1) a dicarboxylic acid component comprising repeat units from at least 80 mole percent of terephthalic acid, and
- (2) a diol component comprising repeat units from 65 to 90 mole percent ethylene glycol and 35 to 10 mole percent 1,4—cyclohexanedimethanol, based on 100 mole percent dicarboxylic acid and 100 mole percent diol; and
- 15 (B) 1 to 10 weight percent of a plasticizer selected from the group consisting of octyl epoxy soyate, epoxy tallates, epoxidized soybean oil, epoxidized linseed oil, triphenyl phosphate, neopentyl glycol dibenzoate, glycerine, vegetable oil, and mineral oil, wherein the combined weights of (A) and (B) total 100 percent; and
  - (II) forming the blend into a film.
  - 14. A polyester/plasticizer concentrate which is used to prepare a heat-shrinkable film comprising:
    - (A) 88 to 94 weight percent of a polyester having a glass transition temperature of 40°C to 150°C and an inherent viscosity of 0.5 to 1.2 dL/g, comprising
    - (1) a dicarboxylic acid component comprising repeat units from at least 80 mole percent of an aromatic dicarboxylic acid having 8 to 14 carbon atoms, and
    - (2) a diol component comprising repeat units from at least 10 mole percent f 1,4-cyclohexanedimethanol, based on 100 mole percent dicarboxylic acid and 100 mole percent diol; and

- 21 -

- (B) 6 to 12 weight percent of a plasticizer selected from a C<sub>4</sub> to C<sub>20</sub> alkyl ester of an epoxidized fatty acid having 12 to 20 carbon atoms provided the plasticizer has sufficient stability to permit its incorporation into the polyester at a temperature of 200°C to 300°C, wherein the combined weights of (A) and · (B) total 100 percent.
- 15. A polyester/plasticizer concentrate which is used to prepare a heat-shrinkable film comprising:
  - (A) 88 to 94 weight percent of a polyester having a glass transition temperature of 40°C to 150°C and an inherent viscosity of 0.5 to 1.2 dL/g, comprising
- (1) a dicarboxylic acid component comprising repeat units from at least 80 mole percent of terephthalic acid, and
  - (2) a diol component comprising repeat units from 65 to 90 mole percent ethylene glycol and 35 to 10 mole percent 1,4-cyclohexanedimethanol, based on 100 mole percent dicarboxylic acid and 100 mole percent diol; and
  - (B) 6 to 12 weight percent of a plasticizer selected from the group consisting of octyl epoxy soyate, epoxy tallates, epoxidized soybean oil, epoxidized linseed oil, triphenyl phosphate, neopentyl glycol dibenzoate, glycerine, vegetable oil, and mineral oil, wherein the combined weights of (A) and (B) total 100 percent.

5

10

15

20

### INILKNATIONAL SEARCH REPORT

Intern: 1 Application No
PCT/US 94/13127

			PC1/US 94/1312/
A. CLASSI IPC 6	FICATION OF SUBJECT MATTER C08K5/15 C08J5/18		
According to	o international Patent Classification (IPC) or to both national class	ification and IPC	•
	SEARCHED		
IPC 6	ocumentation searched (classification system followed by classification COBK COBJ	tion symbols)	
Documentati	tion searched other than minimum documentation to the extent that	such documents are inclu	ided in the fields searched
Electronic di	lata base consulted during the international search (name of data ba	ase and, where practical, s	earch terms used)
C. DOCUM	IENTS CONSIDERED TO BE RELEVANT		
Category*	Citation of document, with indication, where appropriate, of the	relevant passages	Relevant to claim No.
A	EP,A,O 483 757 (DIAFCIL COMPANY) 1992 see claim 1	6 May	1,2
<b>A</b>	WO,A,93 04111 (EASTMAN KODAK COM March 1993 see page 9, line 7 - line 9 see claim 1	1,2	
A	EP,A,O 073 042 (ETHYL CORPORATION 1983) see claims 1-6	N) 2 March	1,2
Furd	ther documents are listed in the continuation of box C.	Patent family r	numbers are listed in annex.
	entegories of cited documents :  ment defining the general state of the art which is not	"T" later document put or priority date an	dished after the international filling date d not in conflict with the application but
"E" earlier filing a "L" docume which	kred to be of particular relevance document but published on or after the international date ent which may throw doubts on priority claim(s) or is cited to establish the publication date of another	invention  "X" document of particle cannot be consider involve an invention  "Y" document of particle	i the principle or theory underlying the ular relevance; the claimed invention ed novel or cannot be considered to ve step when the document is taken alone ular relevance; the claimed invention
'O' docum	n or other special reason (as specified) sent referring to an oral disclosure, use, exhibition or means sent published prior to the international filing date but	document is comb ments, such comb in the art.	red to involve an inventive step when the ined with one or more other such docu- nation being obvious to a person skilled
later ti	han the priority date claimed actual completion of the international search	Date of mailing of	of the same patent family the international search report
8	February 1995	2	4. 02. 95
Name and	mailing address of the ISA  European Patent Office, P.B. 5818 Patentiaan 2  NL - 2280 HV Rijswijk	Authorized officer	
	Td. (+31-70) 340-2040, Tx. 31 651 epo nl, Far (+31-70) 340-3016	Siemens	, Τ΄

# INTERNATIONAL SEARCH REPORT

....ormation on patent family members

Intern: al Application No PCT/US 94/13127

Patent document cited in search report	Publication date		t family iber(s)	Publication date
EP-A-0483757	06-05-92	JP-A- JP-B- US-A-	4164627 6059686 5153302	10-06-92 10-08-94 06-10-92
WO-A-9304111	04-03-93	US-A- EP-A-	5124388 0552171	23-06-92 28-07-93
EP-A-0073042	02-03-83	CA-A- DE-A- JP-T- WO-A- US-A- US-A-	1220594 3277445 58501327 8300697 4486561 4539352	14-04-87 12-11-87 11-08-83 03-03-83 04-12-84 03-09-85

· .		,	